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Key Points:

- A new method for solving the water flow problem is proposed and tested
- The method considers arbitrary network topology, flow direction, and various valve types
- The approach is scalable to large water networks and can be seamlessly integrated for network actuator control and state estimation routines

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A New Derivative-Free Linear Approximation for Solving the Network Water Flow Problem With Convergence Guarantees

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Abstract Addressing challenges in urban water infrastructure systems, including aging infrastructure, supply uncertainty, extreme events, and security threats, depends highly on water distribution networks modeling emphasizing the importance of realistic assumptions, modeling complexities, and scalable solutions. In this study, we propose a derivative-free, linear approximation for solving the network water flow problem. The proposed approach takes advantage of the special form of the nonlinear head loss equations, and, after the transformation of variables and constraints, the water flow problem reduces to a linear optimization problem that can be efficiently solved by modern linear solvers. Ultimately, the proposed approach amounts to solving a series of linear optimization problems. We demonstrate the proposed approach through several case studies and show that the approach can model arbitrary network topologies and various types of valves and pumps, thus providing modeling flexibility. Under mild conditions, we show that the proposed linear approximation converges. We provide sensitivity analysis and discuss in detail the current limitations of our approach and suggest solutions to overcome these. All the codes, tested networks, and results are freely available on Github for research reproducibility.

1. Introduction

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Water distribution networks (WDNs) are complex, large-scale critical infrastructure responsible for providing safe drinking water to the continuously growing population. In the United States, public water utilities serve approximately 95% of the total population (US EPA, 2017). WDNs are composed of numerous elements such as pipes, valves, tanks, and pumps that transport water from a few points of water supply to numerous water consumers. Aging infrastructure, supply uncertainty, growing population, extreme events, and security threats pose mounting challenges on urban water infrastructure (AWWA, 2017; Black & Veatch, 2016). Addressing these challenges depend highly on WDN modeling and the validity of these models. Furthermore, taking advantage of technological advances and integrating smart sensing and actuation with physically based models for operations and management of urban water systems heavily relies on the WDN models. Modeling WDNs involves solving the water flow problem (WFP), which is governed by the *linear* flow continuity and *nonlinear* energy conservation (Todini & Rossman, 2013), and finding the *flow* through each pump, valve, and pipe and *head* at each node given network characteristics, status of pumps and valves, initial head of tanks and reservoirs, and demand at each node of the WDN. Notably, realistic assumptions, modeling complexities, and the inherently large scale of WDNs emphasize the importance of scalable water flow modeling solutions in the context of managing modern WDNs.

The literature of solving the WFP as well as other related problem formulations is rich and briefly summarized next. The main approaches for solving the WFP are based on Hardy-Cross (Cross, 1936), Newton-Raphson (Epp & Fowler, 1970; Liu, 1969; Martin & Peters, 1963; Todini & Pilati, 1987; Wood & Rayes, 1981), linearization (Isaacs & Mills, 1980; Jeppson, 1976; Moosavian, 2017; Price & Ostfeld, 2012; Wood & Charles, 1972; Wood & Funk, 1993), optimization (Arora, 1976; Collins et al., 1978), gradient-based (Todini & Pilati, 1987; Todini & Rossman, 2013), graph decomposition (Deuerlein, 2008; Deuerlein et al., 2009; Diao et al., 2014; Martínez Alzamora et al., 1996), and, more recently, fixed-point methods (Bazrafshan et al., 2018; Zhang et al., 2017). These methods can be classified as primarily relying on iterative updat-

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ing, decomposition methods, or optimization-based formulations, and differ in terms of their modeling limitations and complexity, handling nonlinearities, and convergence speed, as discussed in the following paragraphs.

The first classical approach is attributed to Cross (1936) that developed a loop-based method for solving the WFP suitable for small networks and hand calculations. Martin and Peters (1963) first applied the Newton-Raphson method by modeling all the equations in terms of nodal heads and obtaining the solution via successive iterations. Slow convergence and large oscillations during iterations are the two main disadvantages of the proposed approach. Later, Liu (1969) proposed a simplified version of the Newton-Raphson method via decomposition of the Jacobian matrix into diagonal and nondiagonal matrices, which simplified the solution of the equations. However, the method suffers from convergence issues if the initial guess is not carefully chosen. A linearization method was proposed by Wood and Charles (1972) in terms of link flow equations, where the nonlinear energy equations were linearized and updated in each iteration (Wood & Charles, 1972). Wood and Funk (1993) later extended the link flow model using extended Taylor series. Jeppson (1976) reformulated the nonlinear energy equations for each loop in terms of flow adjustment factors and proposed a linearization method using the standard Taylor series expansion, which was then solved iteratively using the Newton-Raphson method. Isaacs and Mills (1980) proposed a linearization method based on nodal heads providing a simpler model and symmetry of coefficient matrix compared with Wood and Charles (1972). Notably, the global gradient algorithm (Todini & Pilati, 1988) implemented in the EPANET software (Rossman, 2000), which utilizes the Newton-Raphson solution approach for solving the nonlinear system of equations, is the most widely used method for solving the WFP (Burger et al., 2016). Giustolisi et al. (2011) proposed an enhanced global gradient method to accelerate the convergence process for large-scale networks while preserving the accuracy of the solution. Moosavian (2017) derived a multilinear method to improve the convergence rate of Wood and Charles (1972) and Todini and Pilati (1988), where the nonlinear energy equations are linearized based on the maximum and minimum allowable flow rate in pipes and the solution is iteratively updated in the successive iterations. To further accelerate and improve convergence, several recent works have proposed intricate algorithms to exploit network structure in the computational procedure including careful selection of network loops (Alvarruiz et al., 2015; Deuerlein et al., 2015; Vasilic et al., 2018) and selection and decomposition of network trees and forest (Elhay et al., 2014; Simpson et al., 2012).

An alternative approach for solving the WFP is by formulating the problem as nonlinear but convex optimization problem, that is, the content problem that is constrained by linear mass balance equations minimizing network content or the unconstrained dual problem minimizing the cocontent function (Collins et al., 1978; Dembo et al., 1989). The original formulations were later extended to include pressure-dependent demands and flow regulating devices (Deuerlein et al., 2009, 2019; Moosavian & Jaefarzadeh, 2014). The advantages of optimization-based approaches are clear, linear, and convex models can be efficiently solved to global optimality for very large networks using modern solvers (MOSEK ApS, 2014; Gurobi Optimization, Inc. 2014). The approach presented in this paper is most closely related to Sela Perelman and Amin (2015) that initially proposed a geometric programming (GP) approximation (Duffin et al., 1967) for solving the WFP by converting the nonconvex head loss equations into a GP form resulting in a nonlinear but convex optimization problem, and, hence, a globally optimal solution is guaranteed. An important contribution of the previously proposed GP method is that it is noniterative (i.e., a one-shot optimization problem). However, it is only applicable under the assumptions of a tree network topology, known and fixed flow directions, and was limited in the modeling complexities of valves and pumps. These assumptions make the previously proposed approach (Sela Perelman & Amin, 2015) not suitable for urban water networks comprising branched and looped topologies.

In this study, we propose a novel GP approximation-based optimization approach to solve the network flow problem by taking advantage of the special form of the head loss equations. The main advantages and contributions of the proposed approach compared with previous GP-based modelingSela Perelman and Amin (2015) are (1) after transformation of variables and constraints the optimization problem that solves the WFP is linear, (2) any arbitrary topologies and various types of valves and pumps can be seamlessly modeled providing modeling flexibility, and (3) prior knowledge on flow directions or maximum flow rates is not required. Our approach involves two steps: (1) the nonlinear nonconvex WFP is transformed to a nonlinear but convex problem using GP and (2) the convex GP form is further transformed into linear form resulting in a set of linear equations. In short, the proposed approach reduces the WFP to a system of linear equations and

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solves a series of linear programs (LP), thereby graciously scaling to large WDNs. Additionally, we demonstrate that the proposed approach can be straightforwardly extended to model pressure-driven demands and leaks and integrated in control and optimization problems. We provide convergence proof, explore the sensitivy of the approach and propose acceleration scheme for computational speedup. The paper organization is given as follows. Section 2 describes the modeling of WDNs. Section 3 provides some necessary mathematical background related to GP. Section 4 presents the paper's main contribution and the proposed algorithm and Appendix B presents the convergence proof. Section 5 demonstrates the application of our approach to several case studies, and section 6 presents the sensitivity analysis. Section 7 proposes further extensions including pressure-driven modeling and WFP-constrained optimization. Finally, section 8 concludes the paper.

The following notations are used in the text—italicized, boldface upper and lower case characters represent matrices and column vectors: a is a scalar, a is a vector, and a is a matrix. Matrix a denotes the identity square matrix, whereas a0m1 denotes a zero matrix of with size a1 multiplication. The notation a2 denotes the set of real numbers, and notations a2 and a3 denote the sets of column vectors with a4 elements and matrices with a5 elements in a5. For a5 and a7 and a8 compact column vector in a8 defined as a8 and a9 element-wise product is represented as a8 for a9 for a9 for a9. The variables with upper case characters a9, a8, a9, a

2. Modeling of WDNs

A WDN is represented here by a directed graph $\mathcal{G}=(\mathcal{V},\mathcal{E})$. The set \mathcal{V} defines the nodes and is partitioned as $\mathcal{V}=\mathcal{J}\cup\mathcal{T}\cup\mathcal{R}$ where \mathcal{J},\mathcal{T} , and \mathcal{R} stand for the collection of n_j junctions, n_t tanks, and n_r reservoirs, respectively. The set $\mathcal{E}\subseteq\mathcal{V}\times\mathcal{V}$ defines the links and is the partitioned as $\mathcal{E}=\mathcal{P}\cup\mathcal{M}\cup\mathcal{W}$, where \mathcal{P},\mathcal{M} , and \mathcal{W} represent the collection of n_p pipes, n_m pumps, and n_w valves, respectively. The directed graph \mathcal{G} can be expressed by its incidence matrix $\mathbf{A}_{\mathcal{G}}$, which stands for the connection relationship between vertices and edges. For the ith node, the neighboring nodes are defined by the set \mathcal{N}_i , which is partitioned as $\mathcal{N}_i=\mathcal{N}_i^{\mathrm{in}}\cup\mathcal{N}_i^{\mathrm{out}}$, where $\mathcal{N}_i^{\mathrm{in}}$ and $\mathcal{N}_i^{\mathrm{out}}$ collect the nodes of the adjacent inflow and outflow links. Notice that the assignment of direction to each link (and the resulting inflow/outflow node classification) is arbitrary. Thus, $\mathbf{A}_{\mathcal{G}}$ is composed of 1, -1, and 0 elements indicating positive, negative, or no connection, respectively. $\mathbf{A}_{\mathcal{G}}$ can be represented using the block column partition $[\mathbf{A}_h^{\mathcal{P}^T}\mathbf{A}_h^{\mathcal{W}^T}]$, corresponding to pipe, pump, and valve edges, and block row partition $[\mathbf{A}_q^{\mathsf{T}^T}\mathbf{A}_q^{\mathsf{T}^K}^{\mathsf{T}}]^{\mathsf{T}}$, corresponding to junction, reservoir, and tank nodes, as in (1). Note that the dimension of $\mathbf{A}_p^{\mathsf{T}}$ is $n_j \times n_p$, and the size of the other submatrices can be inferred similarly. The details of $\mathbf{A}_{\mathcal{G}}$ are discussed in section 2.2. Table 1 summarizes the variables notation used in this paper.

$$A_{\mathcal{G}} = \begin{array}{c|cccc} Pipe & (n_{p}) & Pump & (n_{m}) & Valve & (n_{w}) \\ \hline Junction & (n_{j}) & A_{p}^{J} & A_{M}^{J} & A_{W}^{J} \\ \hline A_{\mathcal{G}} = & Reservoir & (n_{r}) & A_{p}^{R} & A_{M}^{R} & A_{W}^{R} \\ \hline & Tank & (n_{t}) & A_{p}^{TK} & A_{M}^{TK} & A_{W}^{TK} \\ \hline & A_{p}^{T} & A_{p}^{TK} & A_{M}^{TK} & A_{W}^{TK} \\ \hline \end{array} \right\} A_{q}^{TK}$$

$$(1)$$

2.1. Modeling Components

The basic hydraulic equations describing the flow in WDNs are derived from the principles of conservation of mass and energy (Todini & Rossman, 2013). For elements such as nodes, conservation of mass means the sum of inflows and outflows is equal to 0, and for storage tanks to the change in the water storage volume. The conservation of energy states that the energy difference stored in a component is equal to the energy increases minus energy losses, such as, frictional and minor losses (Puig et al., 2017). According to these basic laws, the equations that model mass and energy conservation for all components in WDNs can be written in explicit and compact matrix-vector forms, as detailed next.

2.1.1. Tanks and Reservoirs

We assume that reservoirs have infinite water supply and the head of the *i*th reservoir is fixed (Gleixner et al., 2012; Singh & Kekatos, 2018; Zamzam et al., 2018) and we have

$$h_i^{\rm R} = h_i^{\rm R_{\rm set}},\tag{2}$$

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Table 1	
Variable Notation	
Notation	Description
$h_i^{\mathrm{J}}, h_i^{\mathrm{R}}, h_i^{\mathrm{TK}}$	Head at the ith junction, reservoir, or tank
$q_{ij}^{\mathrm{P}},q_{ij}^{\mathrm{M}},q_{ij}^{\mathrm{W}}$	Flow through the pipe, pump, or valve from node i to node j
$\Delta h_{ij}^{ ext{P}}, \Delta h_{ij}^{ ext{M}}, \Delta h_{ij}^{ ext{W}}$	Head loss or gain from i to j for the pipe, pump, or valve
s_{ij}	Speed of the pump through node i to node j
o_{ij}	Openness of the valve through node i to node j
ξ	A vector collecting all variables (head and flow)
$\hat{\xi}$	GP form of ξ
$\langle \hat{\xi} \rangle_n$	The <i>n</i> th iteration value of $\hat{\xi}$
$\xi_{ ext{EPANET}}$	Solution provided by EPANET software.
$\xi_{ ext{GP-LP}}$	Solution from our proposed GP-LP-based approach.

where $h_i^{R_{set}}$ is specified.

The head created by a cylindrical tank that has a fixed cross sectional area can be described as

$$h_i^{\rm TK} = h_i^{\rm TK_{set}},\tag{3}$$

where $h_i^{\text{TK}} = \frac{V_i}{A_i^{\text{TK}}} + E_i^{\text{TK}}$ and the elevation E_i^{TK} , volume V_i and cross sectional area A_i^{TK} of the ith tank can be measured

2.1.2. Junctions and Pipes

Junctions are points of connection between links where water flow merges or splits. The expression of mass conservation of the *i*th junction can be written as

$$\sum_{j \in \mathcal{N}_i^{\text{in}}} q_{ji} - \sum_{j \in \mathcal{N}_i^{\text{out}}} q_{ij} = d_i, \tag{4}$$

where d_i stands for end-user demand that is extracted from node i, and we assume that the demand is known for the WFP. The major head loss of a pipe from node i to j is due to friction and is determined by

$$\Delta h_{ii}^{P} = h_i - h_i = R_{ii} q_{ii}^{P} |q_{ii}^{P}|^{\mu-1}, \tag{5}$$

where R_{ij} is pipe resistance coefficient, which is a function of pipe size, length, and material; μ is the constant flow exponent. Note that R_{ij} and μ vary correspondingly with the most common formulae to model the head loss, which are Hazen-Williams, Darcy-Weisbach, and Chezy-Manning (Linsley & Franzini, 1979; Rossman, 2000). The approach presented in this paper considers any of the three formulae. The minor head losses in pipes caused by turbulence that occurs at bends and fittings are not considered in this paper but could be easily modeled using surrogate pipe length.

2.1.3. Pumps

A head increase/gain can be generated by a pump between the suction node i and the delivery node j. The pump properties dictate the relationship function between the pump flow and head increase (Linsley & Franzini, 1979). Generally, the head gain can be expressed as

$$\Delta h_{ij}^{\rm M} = h_i - h_j = -s_{ij}^2 \left(h_0 - r(q_{ij}^{\rm M} s_{ij}^{-1})^{\nu} \right), \tag{6}$$

where h_0 is the shutoff head, $q_{ij}^{\rm M}$ is the flow, $s_{ij} \in (0, s_{ij}^{\rm max}]$ is the relative speed, which is known, and r and v are the curve coefficients of the pump that are chosen from a particular range of values. It is worthwhile to notice that the head gain $h_{ij}^{\rm M}$ is always a negative value and the flow through the pump is always strictly positive. Pump flow and head constraints will be later modeled as operational constraints (10c) and (10b).

2.1.4. Valves

Several types of valves can be utilized to regulate the flows or pressures in WDNs. General Purpose Valves (GPV), Pressure Reducing Valves (PRV), and Flow Control Valves (FCV) are commonly used valves that

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are controlled through valve openness or set points for pressure reduction or flow regulation. The different valve flow-head relationships used in our paper are based on (Rossman, 2000, Chapter 3). GPVs can be used to model turbines, well drawdown, or reduced-flow backflow prevention valves. Here, we assume that the GPVs are modeled similarly to a pipe with controlled resistance coefficient, which can be expressed as

$$\Delta h_{ij}^{W} = h_i - h_j = o_{ij}^{-1} R_{ij} q_{ij}^{W} |q_{ij}^{W}|^{\mu - 1}, \tag{7}$$

where $o_{ij} \in (0,1]$ is a known parameter depicting the openness of a valve, and the rest of the variables are similar to the pipe model. When $o_{ij} = 1$ the valve is fully open and as o_{ij} decreases, the valve closes resulting in greater losses (Piller & van Zyl, 2014). When a GPV is completely closed, no constraint exists between h_i and h_i indicating that the two nodes are decoupled and the corresponding constraint (7) should be removed.

PRVs limit the pressure at a specific location in the network (reverse flow is not allowed) and set the pressure to P^{set} on its downstream side when the upstream pressure is higher than P^{set} (Rossman, 2000, Chapter 3.1); otherwise, they are treated as open pipes with minor head loss. Assuming that the upstream side is denoted as i, and the downstream side is j and given the status of a PRV, the PRV can be modeled as

$$\begin{cases} \Delta h_{ij}^{W} = h_i - h_j = l_{ij} q_{ij}^{W} |q_{ij}^{W}|, \text{OPEN} \\ h_j = h^{W_{\text{set}}}, \text{ ACTIVE}, \end{cases}$$
(8a)

where l_{ij} is the lumped minor head loss coefficient depending on the acceleration of gravity, cross-sectional area, and local losses of the PRV. Parameter $h^{\rm W_{set}}$ is the pressure setting converted to head implying $h^{\rm W_{set}} = E_j + P^{\rm set}$, and E_j is the elevation at junction j, parameter $P^{\rm set}$ is the pressure setting of the PRV and both are constant. Therefore, the head h_j is fixed, and the fact that reverse flow is not allowed in PRVs can be expressed as operational constraint included in (10b). Similarly for GPV, if PRV completely closed, the constraint between the two adjacent nodes h_i and h_j is removed.

FCVs limit the flow to a specified setting $q^{W_{set}}$ when the head h_i at upstream node i is greater than the head h_j at downstream node j, otherwise, FCVs are treated as open pipes with minor head loss. FCVs can be modeled as

$$\begin{cases} \Delta h_{ij}^{W} = h_i - h_j = l_{ij} q_{ij}^{W} |q_{ij}^{W}|, \text{OPEN} \\ q_{ij}^{W} = q^{W_{\text{set}}}, \text{ ACTIVE}, \end{cases}$$
(9a)

where l_{ij} is the lumped minor head loss coefficient and $q^{\mathrm{W}_{\mathrm{set}}}$ is the setting value.

Note that regardless of the type of link, that is, pipe, pump, or valve, a closed indicates that the corresponding flow q_{ij} is 0; thus. the corresponding links are removed from the incidence matrix A_G , and inherently no constraints are imposed between its adjacent nodes i and j.

2.2. Nonlinear WFP Formulation

This section derives an optimization-based formulation given the WDN model. Aside from the physical constraints listed above, typical design and operation problems pertaining to WDNs also consider engineering constraints, such as restricting the desired flows and heads in the network. These additional constraints can be written as

$$h_i^{\min} \le h_i \le h_i^{\max} \tag{10a}$$

$$q_{ij}^{\min} \le q_{ij} \le q_{ij}^{\max} \tag{10b}$$

$$h_{ii}^{\mathrm{M}} \le 0. \tag{10c}$$

Equations (10a) and (10b) are the lower and upper bounds on the heads of nodes, flows through links; equation (10c) is the head increase delivered by pumps. Let the compact vectors \mathbf{h}^{J} , \mathbf{h}^{R} , and \mathbf{h}^{TK} collect the heads at junctions, reservoirs, and tanks, $\mathbf{h} \triangleq \{\mathbf{h}^{\mathrm{J}}, \mathbf{h}^{\mathrm{R}}, \mathbf{h}^{\mathrm{TK}}\}$ collect all the heads at the nodes, where $\mathbf{h} \in \mathbb{R}^{n_h}$ and $n_h = n_j + n_r + n_t$ is the summation of the number of junction, reservoirs, and tanks, respectively.

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Similarly, the flow through pipes, pumps, and valves are collected by compacted vectors \mathbf{q}^P , \mathbf{q}^M , and \mathbf{q}^W , let $\mathbf{q} \triangleq \{\mathbf{q}^P, \mathbf{q}^M, \mathbf{q}^W\}$, and $\mathbf{q} \in \mathbb{R}^{n_q}$, where $n_q = n_p + n_m + n_w$ is the summation of the number of pipes, pumps, and valves, respectively. We define a vector collecting all above optimization variables as $\xi \triangleq \{\mathbf{h}, \mathbf{q}\}$, and $\xi \in \mathbb{R}^{n_\xi}$ where $n_\xi = n_h + n_q$. Thus, all constraints can be summarized as $\xi \in [\xi^{\min}, \xi^{\max}]$, and equations (2)–(9) can be presented as

$$\begin{bmatrix} 0_{n_{j} \times n_{h}} & A_{\mathbf{J}}^{\mathbf{J}} & A_{\mathbf{M}}^{\mathbf{J}} & A_{\mathbf{W}}^{\mathbf{J}} \\ A_{h}^{\mathbf{R}} & 0_{n_{r} \times n_{q}} \\ A_{h}^{\mathbf{TK}} & 0_{n_{r} \times n_{q}} \\ A_{h}^{\mathbf{TK}} & 0_{n_{p} \times n_{p}} \\ A_{h}^{\mathbf{W}} & 0_{n_{m} \times n_{m}} \\ A_{h}^{\mathbf{W}} & 0_{n_{m} \times n_{m}} \\ A_{h}^{\mathbf{W}} & 0_{m} & E \end{bmatrix} \begin{bmatrix} h^{\mathbf{J}} \\ h^{\mathbf{K}} \\ h^{\mathbf{TK}} \\ q^{\mathbf{P}} \\ q^{\mathbf{W}} \end{bmatrix} = \begin{bmatrix} d \\ h^{\mathbf{K}_{act}} \\ h^{\mathbf{TK}_{set}} \\ -\frac{\lambda}{\Delta h} \bar{\mathbf{P}}(q^{\mathbf{P}}) \\ \Delta h^{\mathbf{M}}(q^{\mathbf{M}}) \\ b_{0}^{\mathbf{W}} \end{bmatrix},$$

$$(11)$$

where $\boldsymbol{A}_{\boldsymbol{q}}^{\mathrm{J}} \triangleq [\boldsymbol{A}_{\mathrm{P}}^{\mathrm{J}} \quad \boldsymbol{A}_{\mathrm{M}}^{\mathrm{J}} \boldsymbol{A}_{\mathrm{M}}^{\mathrm{J}}]$ is the mass balance for all nodes (4), $\boldsymbol{A}_{\boldsymbol{h}}^{\mathrm{R}}$ and $\boldsymbol{A}_{\boldsymbol{h}}^{\mathrm{TK}}$ collect (2) and (3) for reservoirs and tanks, $\boldsymbol{A}_{\boldsymbol{h}}^{\mathrm{P}}$ and $\boldsymbol{A}_{\boldsymbol{h}}^{\mathrm{M}}$ collect the head loss equation (5) and the head gain equation (6), and $\boldsymbol{A}_{\boldsymbol{h}}^{\mathrm{W}}$ are the left-hand side of valve (7)–(9). The right-hand side is a vector collecting the corresponding coefficients including demand $\boldsymbol{d} \in \mathbb{R}^{n_j}$ for all junctions, settings of reservoirs $\boldsymbol{h}^{\mathrm{R}_{\mathrm{set}}} \in \mathbb{R}^{n_r}$ and tanks $\boldsymbol{h}^{\mathrm{TK}_{\mathrm{set}}} \in \mathbb{R}^{n_t}$, nonlinear head loss/gain functions for all links $\Delta \boldsymbol{h}^{\mathrm{P}}(\boldsymbol{q}^{\mathrm{P}})$, $\Delta \boldsymbol{h}^{\mathrm{M}}(\boldsymbol{q}^{\mathrm{M}})$, and $\Delta \boldsymbol{h}^{\mathrm{W}}(\boldsymbol{q}^{\mathrm{W}})$ or valve settings $\boldsymbol{h}^{\mathrm{W}_{\mathrm{set}}}$ and $\boldsymbol{q}^{\mathrm{W}_{\mathrm{set}}}$ collected in $\boldsymbol{b}_{0}^{\mathrm{W}}$.

Remark 1. A_0 is a square matrix, and $A_0 \in \mathbb{R}^{n_\xi \times n_\xi}$ since $A_q^{\mathsf{J}} \in \mathbb{R}^{n_j \times n_q}, A_h^{\mathsf{R}} \in \mathbb{R}^{n_r \times n_h}, A_h^{\mathsf{TK}} \in \mathbb{R}^{n_t \times n_h}, A_h^{\mathsf{P}} \in \mathbb{R}^{n_t \times n_h}, A_h^{\mathsf{M}} \in \mathbb{R}^{n_w \times n_h}$, and $A_h^{\mathsf{W}} \in \mathbb{R}^{n_w \times n_h}$.

Assumption 1. A_0 is invertible.

Hence, the overall nonlinear modeling of WFP can be written as

WFP: find
$$\xi$$
 s.t. (10), (11).

The WFP (13) is nonlinear and nonconvex due to the head loss models of pipes and pumps.

Motivated by the literature gaps discussed in section 1 (Sela Perelman & Amin, 2015), we propose a new GP-based optimization approach to solve the WFP, which is convex in the variables, considers various kinds of valves and pumps, while not requiring the a priori knowledge of water flow direction, and applies to any network topology. Note that the GP form itself is not convex, however, the log form of GP is convex. Hence, when we say GP is convex in this paper, we mean that the log form of GP is convex. After the GP is developed, the problem is transformed to an LP, as discussed in section 4.3.

3. GP and Modeling Tricks

A basic introduction to GP is given in this section and a simple LP example is presented to illustrate how to convert a problem into its GP form.

3.1. GP

A geometric program is a type of optimization problem with objective and constraint functions that are monomials and posynomials (Boyd et al., 2007). A real valued function $g(\mathbf{x}) = cx_1^{a_1}x_2^{a_1} \dots x_n^{a_n}$, where c > 0, $\mathbf{x} > 0$, and $a_i \in \mathbb{R}$, is called a *monomial* of the variables x_1, \dots, x_n . A sum of one or more monomials, that is, a function of the form $f(\mathbf{x}) = \sum_{k=1}^K c_k x_1^{a_1k} x_2^{a_2k} \dots x_n^{a_nk}$, where $c_k > 0$, is called a *posynomial* with K terms in the vector variable \mathbf{x} . A standard GP can be written as

GP:
$$\min_{\mathbf{x}>0} f_0(\mathbf{x})$$

s.t. $f_i(\mathbf{x}) \le 1, i = 1, ..., m$ (13)
 $g_i(\mathbf{x}) = 1, i = 1, ..., p$,

where x is an entry-wise positive optimization variable, $f_i(x)$ are posynomial functions, and $g_i(x)$ are monomials. A standard GP form is nonlinear and nonconvex. The main technique to solving a GP efficiently is

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to convert it to a nonlinear but convex problem using a logarithmic change of variables, and a logarithmic transformation of the objective and constraint functions. Defining $y_i = \log x_i$, the log form of GP can be expressed as

GP-log:
$$\min_{\mathbf{y}} \log f_0(\mathbf{y})$$

s.t. $\log f_i(\mathbf{y}) \le 0, i = 1, \dots, m$
 $\log g_i(\mathbf{y}) = 0, i = 1, \dots, p,$

The log form of GP is convex and can be solved efficiently with modern solvers (Boyd et al., 2007, section 2.4). We note that the log function can be with any base *b*, which is greater than 1. With above analysis, we can see that our task is to formulate our WFP as a standard GP, and then the rest can be solved directly by GP solver (Grant & Boyd, 2014; MOSEK ApS, 2014).

3.2. Handling Negative Flows

Since the direction of the flows in the WFP problem is generally unknown, the flow in each pipe can be viewed as free variable, that is, it is unrestricted in its sign. However, all variables in (13) are required to be positive, and reverse direction of flows can not be directly modeled using GP. Several techniques are available to convert the free variables to positive variables, for example, by representing the positive and negative parts by positive dummy variables as in the simplex method (Lustig et al., 1994) for solving LPs. However, this modeling trick does not apply in our setting (see (5) and (7)). Here, we propose another trick to convert a free variable to a positive one, thus allowing modeling reverse direction of flows. Consider an exponential function $f(x) = b^x$ that can map any x to f(x) and f(x) is always positive. Taking advantage of this idea, we can convert a problem with a negative feasible region into a new problem with a positive feasible region. After the solution of the transformed problem is obtained, the original solution can be obtained simply by reverting back. For ease of demonstration, we illustrate this idea using a simple LP problem (14).

First, the original free variables are converted into the corresponding GP variables denoted using \hat{x} , for example, the variables x_1 and x_2 turn into \hat{x}_1 and \hat{x}_2 via $\hat{x}_1 = b^{x_1}$ and $\hat{x}_2 = b^{x_2}$, where the base b > 1. Second, the constraints and objective functions are converted into the monomial or posynomial form, for example, the constraint $-x_1 + x_2 \le 4$ can be expressed as $b^{-4} \hat{x}_1^{-1} \hat{x}_2^1 \le 1$ via executing exponential on both sides of $-x_1 + x_2 \le 4$. Thus, we successfully convert an LP (14) into its GP form (15) and the solution of the original LP problem can also be obtained using GP solver.

$$\min 2x_1 + 3x_2
s.t. - x_1 + x_2 \le 4$$
(14)

$$\min \hat{x}_{1}^{2} \hat{x}_{2}^{3}$$
s.t. $b^{-4} \hat{x}_{1}^{-1} \hat{x}_{2}^{1} \le 1$ (15)

Any LP problem can be converted; however, the conversion of LP seems to make the transformed problem harder. This is not the case when the nominal problem is highly nonlinear and nonconvex. The technique we introduced may help to transform a nonconvex, nonlinear problem into a convex one as shown in subsequent sections.

4. GP Modeling and Corresponding LP Modeling of WFP

Based on the new introduced optimization technique, we convert the nonlinear WFP (13) into its GP form, then derive the corresponding LP model, and propose an algorithm to solve the GP-LP problem.

4.1. Conversion of Variables

Here, the GP variables $\hat{\xi}$ are obtained by mapping the optimization variables ξ in (13). Specifically, we convert the head and demand at the ith node, h_i and d_i , and the flow q_{ij} into positive values \hat{h}_i , \hat{d}_i , and \hat{q}_{ij} through exponential functions, as follows

$$\hat{h}_i \triangleq b^{h_i}, \ \hat{d}_i \triangleq b^{d_i}, \ \hat{q}_{ii} \triangleq b^{q_{ij}}, \tag{16}$$

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where $b = 1 + \delta$ is a constant base and δ is a small positive number. The variables \hat{h}_i , \hat{d}_i , and \hat{q}_{ij} are positive, which can then be used to transform the nonconvex WFP (13) into a GP.

4.2. Conversion of Mass and Energy Balance Equations

4.2.1. Mass Balance Equations for Junctions

Converting mass balance at junctions following the above exponential mapping (16) is straightforward. After exponentiating both sides of (4), variables collected in ξ are changed into $\hat{\xi}$, the summation is turned into multiplication, and we obtain

$$\sum_{b' \in \mathcal{N}_i^{\text{in}}} q_{ji} - \sum_{j \in \mathcal{N}_i^{\text{out}}} q_{ij} = \prod_{j \in \mathcal{N}_i^{\text{in}}} b^{q_{ji}} \prod_{j \in \mathcal{N}_i^{\text{out}}} b^{-q_{ij}} = \prod_{j \in \mathcal{N}_i^{\text{in}}} \hat{q}_{ji} \prod_{j \in \mathcal{N}_i^{\text{out}}} \hat{q}_{ij}^{-1} = b^{d_i} = \hat{d}_i.$$

After the transformation, constraint (4) is converted to monomial equality constraint written as

$$\prod_{j \in \mathcal{N}_i^{\text{in}}} \hat{q}_{ji} \prod_{j \in \mathcal{N}_i^{\text{out}}} \hat{q}_{ij}^{-1} \hat{d}_i^{-1} = 1.$$
 (17)

4.2.2. Energy Balance Equations for Pipes

Now we convert the head loss model for pipes and let $\Delta \hat{h}_{ij}^{P}$ be the GP form of head loss of a pipe, which is obtained by exponentiating both sides of (5) as follows

$$\hat{h}_i \hat{h}_i^{-1} = \Delta \hat{h}_{ij}^{P} = b^{\left(q_{ij}^P R_{ij} | q_{ij}^P|^{\mu-1} - q_{ij}^P + q_{ij}^P\right)} = b^{q_{ij}^P \left(R_{ij} | q_{ij}^P|^{\mu-1} - 1\right)} \quad \hat{q}_{ij} = \hat{c}^P (q_{ij}^P) \quad \hat{q}_{ij}^P,$$

where $\hat{c}^{\mathrm{P}}(q_{ij}^{\mathrm{P}}) = b^{q_{ij}^{\mathrm{P}}\left(R|q_{ij}^{\mathrm{P}}|^{\mu-1}-1\right)}$ is a function of q_{ij}^{P} , which means $\hat{c}^{\mathrm{P}}(q_{ij}^{\mathrm{P}})$ can be viewed as a known when q_{ij}^{P} is given. At first, we can make an initial guess denoted by $\langle q_{ij}^{\mathrm{P}}\rangle_0$ for the 0th iteration $(\langle \hat{c}^{\mathrm{P}}\rangle_0$ can be obtained if $\langle q_{ij}^{\mathrm{P}}\rangle_0$ is known), thus, for the nth iteration, the corresponding values are denoted by $\langle q_{ij}^{\mathrm{P}}\rangle_n$ and $\langle \hat{c}^{\mathrm{P}}\rangle_n$. If the flow rates are close to each other between two successive iterations, we can approximate $\langle \hat{c}^{\mathrm{P}}\rangle_n$ using $\langle \hat{c}^{\mathrm{P}}\rangle_{n-1}$, that is $\langle \hat{c}^{\mathrm{P}}\rangle_n \approx \langle \hat{c}^{\mathrm{P}}\rangle_{n-1}$. Then, for each iteration n,

$$\langle \hat{c}^{\rm P} \rangle_n = b^{\langle q_{ij}^{\rm P} \rangle_{n-1} \left(R | \langle q_{ij}^{\rm P} \rangle_{n-1} |^{\mu-1} - 1 \right)}$$

can be approximated given the flow value $\langle q_{ij}^P \rangle_{n-1}$ from the previous iteration. With this approximation, the head loss constraint for each pipe can be written as a monomial equality constraint

$$\hat{h}_i \hat{h}_i^{-1} [\hat{c}^P]^{-1} [\hat{q}_{ij}^P]^{-1} = 1. \tag{18}$$

The idea is to iteratively update the above monomial equality constraint, where the highly nonlinear term is included into a parameter \hat{c}^P and computed based on the solution of the previous iteration. The new obtained solution is used to update \hat{c}^P again and generate the constraints in next iteration. This technique is similar to the iterative update in the gradient and Newton-Raphson approaches (Todini & Pilati, 1987).

4.2.3. Energy Balance Equations for Pumps

Similarly, the new variables $\hat{q}_{ij}^{\mathrm{M}} = b^{q_{ij}^{\mathrm{M}}}$ and $\hat{s}_{ij} = b^{s_{ij}}$ for $(i,j) \in \mathcal{M}$ are introduced for pumps. Let $\Delta \hat{h}_{ij}^{\mathrm{M}}$ be the GP form of head increase of a pump:

$$\hat{h}_{i}\hat{h}_{j}^{-1} = \Delta \hat{h}_{ij}^{M} = b^{-s_{ij}^{2}(h_{0}-r\ (q_{ij}^{M})^{\nu}s_{ij}^{-\nu})} = b^{-s_{ij}^{2}h_{0}} \quad (b^{q_{ij}^{M}})^{r(q_{ij}^{M})^{\nu-1}s_{ij}^{2-\nu}} = \hat{c}_{1}^{M}(\hat{q}_{ij})^{c_{2}^{M}}, \tag{19}$$

where $\hat{c}_1^{\mathrm{M}} = b^{-s_{ij}h_0}$ and $c_2^{\mathrm{M}} = r(q_{ij}^{\mathrm{M}})^{\nu-1}s_{ij}^{2-\nu}$. Parameters \hat{c}_1^{M} and c_2^{M} follow a similar iterative process as \hat{c}^{P} . That is, they are treated at the nth iteration as constants based on the flow and relative speed values at the n-1th iteration. Hence, the approximating equation for the pump head increase becomes the monomial equality constraint

$$\hat{h}_i \hat{h}_j^{-1} [\hat{q}_1^{\mathrm{M}}]^{-1} [\hat{q}_{ij}^{\mathrm{M}}]^{-c_2^{\mathrm{M}}} = 1.$$
 (20)

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4.2.4. Energy Balance Equations for Valves

As for valves, the derivation of GPVs is the same as for pipes except for an extra variable $\hat{o}_{ij} = b^{o_{ij}^{-1}}$ for $(i, j) \in \mathcal{W}$ is introduced. Let $\Delta \hat{h}_{ij}^{W}$ be the GP form of head loss of a valve, which is obtained by exponentiating both sides of (7) as follows.

$$\hat{h}_i \hat{h}_j^{-1} = \hat{h}_{ij}^{\mathrm{W}} = b^{\left(o_{ij}^{-1} q_{ij}^{\mathrm{W}} R | q_{ij}^{\mathrm{W}}|^{\mu-1} - q_{ij}^{\mathrm{W}} + q_{ij}^{\mathrm{W}}\right)} = b^{o_{ij}^{-1} \left(R q_{ij}^{\mathrm{W}} | q_{ij}^{\mathrm{W}}|^{\mu-1} - q_{ij}^{\mathrm{W}}\right)} \quad \hat{q}_{ij} = \hat{c}^{\mathrm{W}} \quad \hat{q}_{ij},$$

where $\hat{c}^{W}(q_{ij}^{W}) = b^{o_{ij}^{-1}q_{ij}^{W}\left(R|q_{ij}^{W}|^{\mu-1}-1\right)}$ is a similar parameter as the parameters in pipe and pump models. Hence, the monomial equality constraint can be used for GPVs

$$\hat{h}_i \hat{h}_j^{-1} [\hat{c}^{W}]^{-1} \left[\hat{q}_{ij}^{W} \right]^{-1} = 1.$$
 (21)

For PRVs and FCVs, the conversion process is similar as the one of pipes or GPVs, and equations (22) and (23) can be obtained after exponentiating both sides of (8) and (9).

$$\begin{cases} \hat{h}_{i}\hat{h}_{j}^{-1} \left[\hat{c}^{W}\right]^{-1} \left[\hat{q}_{ij}^{W}\right]^{-1} = 1, \text{ OPEN} \\ \hat{h}_{j}^{-1}\hat{h}^{W_{\text{set}}} = 1, \text{ ACTIVE} \end{cases}$$
 (22a)

$$\begin{cases} \hat{h}_i \hat{h}_j^{-1} [\hat{c}^W]^{-1} [\hat{q}_{ij}^W]^{-1} = 1, \text{ OPEN} \\ [\hat{q}_{ij}^W]^{-1} \hat{q}^{W_{\text{set}}} = 1, \text{ ACTIVE} \end{cases}$$
 (23a)

where $\hat{c}^{W}(q_{i:}^{W}) = b^{q_{ij}^{W}(l_{ij}|q_{ij}^{W}|-1)}$ in (22) and (23).

4.2.5. Physical Constraints

For the physical constraints (10), the conversion process is similar to section 4.2.1 since both are linear constraints. After exponentiating (10), the GP form becomes

$$\hat{h}_i^{-1} \hat{h}_j^{\min} \le 1, \hat{h}_i \left[\hat{h}_j^{\max} \right]^{-1} \le 1$$
 (24a)

$$\hat{q}_{ij}^{-1} \hat{q}_{ij}^{\min} \le 1, \hat{q}_{ij} \left[\hat{q}_{ij}^{\max} \right]^{-1} \le 1$$
 (24b)

$$\hat{h}_{ij}^{\mathrm{M}} \le 1. \tag{24c}$$

4.2.6. GP Modeling of WFP

After the conversion of all variables and constraints, we can express the converted problem as

WFP-GP: find
$$\hat{\xi}$$

s.t. (17) – (24).

Problem (26) is in standard GP form and can be solved directly by modern GP solvers and even though the WFP-GP (26) is not convex, as we mentioned, the log form of this problem is convex(Boyd et al., 2007, section 2.5). Starting with an initial guess for the flow rates and relative speeds, the constraints (17)–(24) are approximated at every iteration based on the previous iterations. This process continues until a termination criterion is met. The details are further discussed in Algorithm 1. In the next section, we show how the WFP-GP (26) problem can be formulated using a tractable linear approximation.

4.3. LP Modeling Derived From GP Modeling

As we illustrated in the end of section 3, an LP and a GP can be converted to each other; for example, equation (15) can be obtained from (14) via exponent technique, and the inverse operation also holds true meaning that equation (14) can be converted back from (15) via the log operator. Inspired by this idea, we can apply the inverse operation to WFP-GP (26), and generate an LP for the WFP. After applying the log function on both sides of GP form of the mass balance Equation (17), the result would be the original linear

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form of the mass balance equation (4). It means the linear modeling is converted back from GP modeling. Similarly, for equations (22)–(24), the corresponding results are (8)–(10).

As for the GP form of energy balance equations for pipes, after applying the log function with base b on both sides of equation (18), a linear equation can be obtained as

$$h_i - h_j - q_{ij}^{P} = c_{ij}^{P}, (26)$$

where $c_{ij}^{P} = \log_b(\hat{c}_{ij}^{P})$.

Similarly, the linear form of energy equation balance for pumps and valves (GPVs, PRVs, and FCVs) can be expressed as (27) and (28) when applying the log function on both sides of (20), (21), (22a), and (23a), as

$$h_i - h_j - c_2^{\mathrm{M}} q_{ij}^{\mathrm{M}} = c_1^{\mathrm{M}} \tag{27}$$

$$h_i - h_j - q_{ij}^{W} = c_{ij}^{W}, (28)$$

where $c_1^{\rm M} = \log_b(\hat{c}_1^{\rm M})$ and $c_{ij}^{\rm W} = \log_b(\hat{c}_{ij}^{\rm W})$. Note that $(i)\hat{c}_{ij}^{\rm W}$ varies according to the types of valves, (ii) equation (28) applies to PRVs and FCVs in open status, and for active status, equations (8b) or (9b) is used, which are linear as well. Thus, the nonlinearities from pipes (5), pumps (6), and valves (GPVs (7), PRVs (8), and FCVs (9)) are approximated by its linear form (26)–(28).

After updating the model in (11), the linear matrix representation of WDNs can be written as

$$\begin{array}{c}
A^{J} \leftarrow \\
A^{R} \leftarrow \\
A^{R} \leftarrow \\
A^{K} \leftarrow \\
A^{TK} \leftarrow \\
A^{P} \leftarrow \\
A^{D} \leftarrow \\
A^{D} \leftarrow \\
A^{D} \leftarrow \\
A^{M} \leftarrow \\
A^{M} \leftarrow \\
A^{M} \leftarrow \\
A^{W} \leftarrow
\end{array}$$

$$\begin{array}{c}
A_{D}^{J} A_{M}^{J} A_{M}^{J} A_{W}^{J} \\
0_{n_{f} \times n_{q}} \\
0_{n_{f} \times n_{q$$

where c^{P} , c_{1}^{M} , C_{2}^{M} , and b^{W} collect the parameters from linear modeling of pipes, pumps, and valves, and note that $c^{P} \in \mathbb{R}^{n_{p}}$, c_{1}^{M} and $c_{2}^{M} \in \mathbb{R}^{n_{m}}$, $c_{2}^{M} = diag(c_{2}^{M}) \in \mathbb{R}^{n_{m} \times n_{m}}$, and $b^{W} \in \mathbb{R}^{n_{w}}$ including c^{W} or valve settings $h^{W_{\text{set}}}$, $q^{W_{\text{set}}}$. Thus, the LP form of WFP can be expressed as

WFP-LP: find
$$\xi$$

s.t. (10), (29).

Remark 2. A in (29) is a square matrix, and $A \in \mathbb{R}^{n_{\xi} \times n_{\xi}}$ since two zero submatrices in A_0 (11) are replaced with the matrices $-I_{n_p \times n_p}$ and C_2^M with the same size.

Lemma 1. A is invertible. The proof is given in AppendixA.

WFP-LP (30) derived from GP form can be viewed as a linear approximation of nonlinear WFP modeling (13), and it can be solved with any LP solvers directly. Note that all constraints of (30) are equality constraints except the lower and upper bounds in (10), and we can rewrite them in matrix form

$$A[\underline{A^{J}; A^{R}; A^{TK}; A^{P}; A^{M}; A^{W}}]\xi = b[\underline{b^{J}; b^{R}; b^{TK}; b^{P}; b^{M}; b^{W}}],$$
(31)

where A is a coefficient matrix collecting all submatrices and A^{I} is from the mass balance equation (4), A^{R} and A^{TK} collects (2) and (3) for reservoirs and tanks, A^{P} is from the linearized pipe head loss equation (26), A^{M} is linearized equation (27) for pump, and A^{W} collects all linear equations for valves. The right-hand side b is a coefficient vector collecting the corresponding coefficients in (29). An example of A and b is given in section 5

We note that A is square, invertible matrix (Lemma 1), which implies that an analytical solution can be obtained efficiently large-scale networks using scalable methods for solving linear systems of equations.

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Algorithm 1: GP-LP method for solving the WFP



The bound constraints (10) are not including in this case, since these constraints are included in design and operation problems to adjust for admissible flows and heads. We will illustrate later in the paper that this approach yields good performance, in comparison with solving a linear program with inequality constraints (10).

Next, we provide Algorithm 1 for solving the WFP using WFP-LP (30) or its matrix form (31). Notice that all variables are collected in ξ and the notation $\langle \xi \rangle_n$ in Algorithm 1 stands for the *n*th iteration value ξ . The initial statuses of pumps and valves, head in tanks, and reservoirs as well as nodal demands are assumed to be known. For the users familiar with the EPANET software (Rossman, 2000), all the necessary information needed to formulate the WFP-LP (30) can be seamlessly imported from the ".inp" source file.

```
Input: WDN characteristics/.inp source file, initial guess \langle \xi \rangle_0, threshold, maxIter, n_{\text{step}} Output: \xi_{\text{GP-LP}}

1 Set \xi_{\text{save}} := \langle \xi \rangle_0, n = 1, generate A and b using (31)

2 while error \geq threshold \ OR \ n \leq maxIter \ do

3 Determine the status of each pump and valve and obtain \langle \mathbf{c}^P \rangle_n, \langle \mathbf{c}_2^M \rangle_n, and \langle \mathbf{c}^W \rangle_n from \langle \xi \rangle_{n-1}
```

```
Update part of A, b, and solve for \langle \xi \rangle_n = A^{-1}b

if mod(n, n_{step}) = 0 then

\Delta \xi = \langle \xi \rangle_n - \langle \xi \rangle_{n-1}
\langle \xi \rangle_n = \langle \xi \rangle_{n-1} + a_n \circ \Delta \xi
end if

Calculate error := norm(\langle \xi \rangle_n, \xi_{save})
Update \xi_{save} = \langle \xi \rangle_n and n = n + 1

11 end while
```

Algorithm 1 is initialized with any initial guess $\langle \xi \rangle_0$ and requires defining the threshold or number iterations for convergence as well as acceleration parameter a_n . In each iteration, parameters $\langle c^p \rangle_n$ and $\langle c^W \rangle_n$ are updated based on previous iterations, $\langle c_2^M \rangle_n$ is fixed and does not need to be updated, and matrices A and b collecting the above parameters are automatically updated as well. Notably, for a fixed topology only submatrices A^P , A^M , and parts of A^W and the corresponding parts in vector b require updating, while the rest remain fixed. The iteration error is defined as the Euclidean distance between two consecutive iterations. The iterations continue until the error is less than a predefined error threshold (threshold) or the maximum number of iterations (maxIter) is reached, and the final solution is set by $\xi_{GP-LP} = \langle \xi \rangle_n$.

Steps 5–8 are used to accelerate the convergence of the algorithm. The acceleration parameter a_n that can be adjusted dynamically with iterations, for example, every n_{step} iterations, and set individually for different elements, where $a_n \circ \Delta \xi$ represents element-wise product. Algorithm 1 can also be applied to solve the optimization problem (26) or (30) with corresponding GP/LP solver. When dealing with (26), the steps remain the same except that the variables are changed into the GP variables $\hat{\xi}$. For the same scale problem, the GP solver is usually slower than an LP solver, and the analytical solution is faster than any solver.

4.4. Convergence of GP-LP Iteration

12 Let $\xi_{\text{GP-LP}} = \langle \xi \rangle_n$

In Appendix B, we show the convergence of proposed GP method under mild conditions that typically hold in practical WDNs. The theorem and proof are given first, followed by a discussion on how the initial points and acceleration parameter in Algorithm 1 are related with the convergence. Specifically, we note that a large a_n can be set for a pipe with small R_{ij} , a_n is related to not only the flow rate but also to the change of flow rate in the (n-1)th iteration, and when $\langle \Delta q_i^P \rangle_{n-1}$ converges to 0, a_n can theoretically be infinity. In Appendix B, we give bounds to limit a_n in each iteration by (B8a) and (B8b) simultaneously. The acceleration parameter a_n that is not limited by the given range can cause the iterations to oscillate or diverge and, hence, a large acceleration parameter can make the iterations less stable. It follows that a proper choice of a_n is needed for each element and iteration to reach the best performance of convergence. Although beyond the scope of this work, the convergence can be optimized by adopting self-adaptation acceleration parameter (Solomon & Van Hemmen, 1996).

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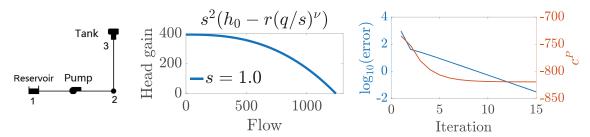


Figure 1. Three-node network (left), variable-speed pump curve (middle), and the value of $\log_{10}(error)$ and c^P during iterations (right).

5. Case Studies

Four WDN examples (three-node, eight-node, Anytown, and C-Town networks) are used to illustrate in detail the applicability of the GP-LP approximation for solving the WFP, and three additional networks are used to test the convergence and simulation times. The first testcase, that is, the three-node network, is developed to illustrate the details of GP-LP model. The second case is a modified eight-node network with a PRV to illustrate that proposed approach is able to handle looped topologies and valves. The C-Town network is used to test the scalability of our approach, and the Anytown network is adopted to discuss the sensitivity analysis. The numerical tests simulated and compared with the help of the EPANET Matlab Toolkit (Elíades & Kyriakou, 2009) on a MacBook Pro with an Intel Core i7 at 2.2 GHz. No acceleration parameter is used except for the sensitivity analysis of the Anytown network, and different threshold and maximum iterations are set for each network. All the results reported in the next sections are based on solving the LP matrix form of the WFP. All codes, parameters, tested networks, and results are available on github (GP-NET, 2019).

5.1. Illustrative Three-Node Network

In this example, the network is composed of three nodes (one reservoir, one tank, and one junction with demand) as shown in Figure 1 (left). The corresponding model can be written as (33) in Table 2. The heads at Reservoir 1 and Tank 3 are $h_1^{R_{\text{set}}} = 213.4$ m, and $h_3^{TK_{\text{set}}} = 276.8$ m; the demand at Junction 2 is $d_2 = 276.8$ 6.3×10^{-3} m³/s. The curve of variable-speed pump is shown in Figure 1 (middle), the relative speed is known and fixed at $s_{12}=1$, and the other parameters are $h_0=393.7$, $r=3.8288\times 10^{-6}$, and $\nu=2.59$. Note that curve of the pump in Figure 1 (middle) is the negative value of Δh^M defined in (6). Given the length $L^P = 304.8$ m, diameter $D^P = 0.304$ ft, and coefficient $C_{HW} = 100$, the resistance coefficient is $R_{23} = 1.145 \times 10^{-5}$. The upper and lower bound constraints are expressed by (33e) to save space.

5.1.1. Nonlinear Modeling of Three-Node Network

In the problem expressed by equation (33), there are a total of six variables, which can be reduced to three variables because two of them $(h_1, \text{ and } s_{12})$ are fixed, and h_3 represents the water surface elevation because the system is assumed to be operated under steady conditions. The variable h_2 can be eliminated by adding (33c) and (33d). Hence, finding the feasible solution of (33) equals to solving the following nonlinear equations

$$\begin{cases} h_3 = h_1^{R_{\text{set}}} - R_{23} q_{23} |q_{23}|^{\mu-1} + (h_0 - r(q_{12})^{\nu}) \\ 0 = q_{12} - q_{23} - d_2 \\ h_3 = h_2^{\text{TK}_{\text{set}}}. \end{cases}$$
(32a)
$$(32b)$$

$$(32c)$$

$$0 = q_{12} - q_{23} - d_2 (32b)$$

$$h_3 = h_3^{\text{TK}_{\text{set}}}. (32c)$$

The problem represented by (32), which can be visualized in Figure 2 where each constraint is represented by a corresponding plane. The solution lies in the intersection of surfaces defined by (32a)–(32c).

5.1.2. GP-LP Modeling of Three-Node Network

The corresponding GP formulation of (33) is listed in (34) in Table 2 after applying the technique we introduced in section 3.1. As we mentioned in section 4.3, the GP can be transformed to an LP via performing the log function, as shown in (35) in Table 2. Furthermore, (36) is obtained after rewriting (35) in matrix form. We can see that (35) is a linear approximation, but not the same as the first-order Taylor approximation. Now this problem can be solved by an LP solver directly. The parameters we use in Algorithm 1 for the three-node network are selected as threshold = 0.01 and maxIter = 100. Figure 1 (right) shows how the error decreases and c^{P} is updated in each iteration until convergence, which occurs in n = 15 iterations.

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Table 2 Three-Node Network Formulation							
Find ξ	Original form	Find $\hat{\xi}$	GP form				
s.t. $q_{12} - q_{23} = d_2$	(33a)	s.t. $\hat{q}_{12} \ \hat{q}_{23}^{-1} \ \hat{d}_2^{-1} = 1$	(34a)				
$h_1 = h_1^{R_{\text{set}}}, \ h_3 = h_3^{\text{TK}_{\text{set}}}$	(33b)	$\hat{h}_1^{-1}\hat{h}_1^{\mathrm{R}_{\mathrm{set}}} = 1, \ \hat{h}_3^{-1}\hat{h}_3^{\mathrm{TK}_{\mathrm{set}}} = 1$	(34b)				
$h_2 - h_3 = R_{23} \ q_{23} \ q_{23} ^{\mu - 1}$	(33c)	$\hat{h}_2 \ \hat{h}_3^{-1} \ [\hat{c}^P]^{-1} \ \hat{q}_{23}^{-1} = 1$	(34c)				
$h_1 - h_2 = -(h_0 - r(q_{12})^{\nu})$	(33d)	$\hat{h}_1 \ \hat{h}_2^{-1} [\hat{c}_1^{\rm M}]^{-1} (\hat{q}_{12})^{-c_2^{\rm M}} = 1$	(34d)				
$\xi \in [\xi^{\min}, \xi^{\max}]$	(33e)	$\hat{\xi} \in [\hat{\xi}^{\min}, \hat{\xi}^{\max}],$	(34e)				
Find ξ	LP form	Find ξ	LP matrix form				
s.t. $q_{12} - q_{23} = d_2$	(35a)	$\begin{bmatrix} 0 & 0 & 0 & 1 & -1 & \end{bmatrix} \begin{bmatrix} h_2 & 1 & k_{\text{set}} \end{bmatrix}$					
$h_1 = h_1^{R_{\text{set}}}, \ h_3 = h_3^{\text{TK}_{\text{set}}}$	(35b)	$\begin{bmatrix} 0 & 0 & 0 & 1 & -1 \\ 0 & 1 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 & 0 \\ 1 & 0 & -1 & -1 & 0 \end{bmatrix} \begin{bmatrix} h_2 \\ h_1 \\ h_3 \\ gas \end{bmatrix} = \begin{bmatrix} a_2 \\ h_1^{K_{Set}} \\ h_1^{K_{Ket}} \\ h_3^{T} \end{bmatrix}$					
$h_2 - h_3 = c^{P} + q_{23}$	(35c)	$\begin{bmatrix} 1 & 1 & 0 & 0 & -c^{M} \end{bmatrix} \begin{bmatrix} \frac{4}{3} & 23 & 0 \\ \frac{4}{3} & 23 & 0 \end{bmatrix} \begin{bmatrix} c^{4} & 1 & 0 \\ 0 & 1 & 0 \end{bmatrix}$	(36)				
$h_1 - h_2 = c_1^{\mathrm{M}} + c_2^{\mathrm{M}} q_{12}$	(35d)	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$					
$\xi \in [\xi^{\min}, \xi^{\max}],$	(35e)	A ξ b					

In order to show that our method converges from random initial points, we generate 40 random values for q_{12} and q_{23} , and all of them converge to the same final value. We plot the trajectory of Algorithm 1 from random initial guesses to the final solution, represented by the colorful lines in Figure 2, where the marker represents the value of the initial guess, in terms of flow and head, and the color of the line represents the two-norm distance of current value, where red and blue represent initial guesses farther and closer to the final solution, respectively. We can see that regardless of the initial value, the solution converges to the final value (blue and small marker). Similar random initializations were performed in the rest of the networks presented in this work demonstrating convergence to the correct solution regardless of the initial guess. We compare our solution to EPANET simulations and the obtained results are listed in Table 3. The absolute error between $\xi_{\rm GP-LP}$ and $\xi_{\rm EPANET}$ is defined as $AE = |\xi_{\rm GP-LP} - \xi_{\rm EPANET}|$, the corresponding relative error is $RE = \frac{AE}{|\xi_{\rm EPANET}|} \times 100\%$, and the Euclidean norm $EN = ||\xi_{\rm GP-LP} - \xi_{\rm EPANET}||$. The results show that the our approach performs well for this simple tree topology-based network.

5.2. Modified Eight-Node Network

The eight-node network is adopted from Rossman, (2000, Chapter 2) and includes a PRV to test our approach with control valves. The modified version includes three more junctions (Nodes 9–11) and a PRV between Junctions 3 and 9. Labels for various components and the topology of modified eight-node network are shown in Figure 3a. A PRV has two different states corresponding to its working condition. When the PRV is working in "ACTIVE" condition, the pressure setting is $P^{\text{set}} = 45$ m. The elevation at downstream side is $E_9 = 190$ m. The constraint determined by this PRV from (8) is $h_9^{\text{W}} = 235$ m. The parameters for Algorithm 1 are set as: threshold = 0.01 and maxIter = 100. We test both the "ACTIVE" scenario when pressure setting is 45 m or 100 m and the "OPEN" scenario. The error in the three tested scenarios compared to EPANET

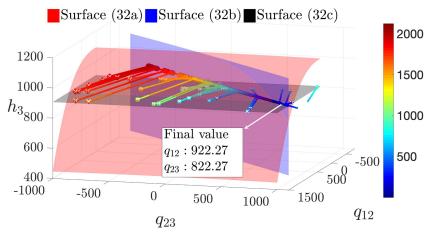


Figure 2. Visualization of the iteration process for 40 random initial points (x markers).

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Table 3								
Solution of Three-Node Network GP-LP Versus EPANET								
Variables	$\xi_{ ext{GP-LP}}$	$\xi_{ ext{EPANET}}$	RE	EN				
h ₂ (m)	277.6330	277.6316	0.0005%					
q_{12} (m ³ /s)	5.8186×10^{-2}	5.8186×10^{-2}	0%	1.4021×10^{-3}				
q_{23} (m ³ /s)	5.1877×10^{-2}	5.1877×10^{-2}	0%					

simulation results is EN = 0.0067. The problem for this test case has a 23 \times 23 A matrix standing for 23 LP variables and 23 LP constraints when rewritten in the LP matrix form. The difference in number of constraints stems from not considering the upper and lower bound constraints when the network is modeled in the LP matrix form.

5.3. C-Town Network

In order to test the scalability of our proposed GP-LP approach, we test the C-Town network (Ostfeld et al., 2012) that contains 364 junctions, 1 reservoir, 7 tanks, 405 pipes, 11 pumps (three of them are in "closed" status), and 4 valves (one of them is closed) shown in Figure 3c. The size of \boldsymbol{A} is 783×783, and the parameters for Algorithm 1 are set as: threshold = 0.01 and maxIter = 1000.

Figure 4 (left) shows the log(EN) with iterations, and Figure 4 (right) shows the histogram of absolute errors of individual network components. Note that the convergence criteria is defined as the Euclidean norm between $\xi_{\text{GP-LP}}$ and ξ_{EPANET} , which summarizes the values of all the components and not individual components. At the final iteration, EN = 1.6969, which pertains to a 783 × 1 vector; thus, the error per variable is small. The histogram in Figure 4 (right) shows that 99% of absolute errors are within [0, 0.5].

The computational time of solving the LP in matrix form is approximately 5 s with a highly sparse 783×783 matrix \boldsymbol{A} in C-Town, where 99.66% of the elements are zeros. The computational time could be further reduced by applying efficient methods for solving \boldsymbol{A}^{-1} . Note that this is preliminary work for modeling WDNs, and the majority of computational time involves reading input files, preparing the parameters, and saving temporary results. The code will be optimized in the future work.

5.4. Computational Time Statistics for Tested Cases

We tested the proposed algorithm using additional WDNs that vary in their size and complexity, including PES, NPCL, and OBCL (Eliades et al., 2016). Summary of the main WDNs properties and simulation results

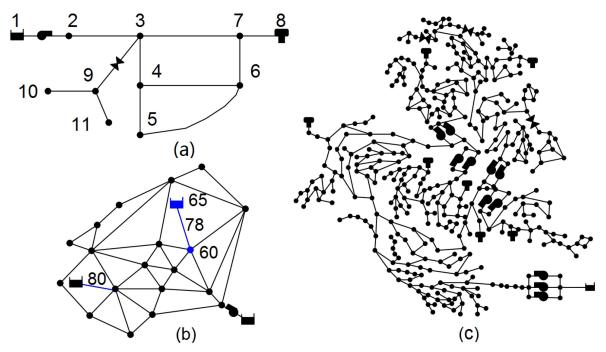


Figure 3. (a) Modified eight-node network, (b) Anytown, and (c) C-Town network.

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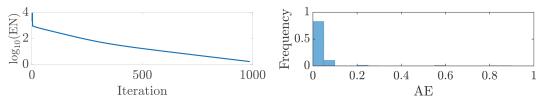


Figure 4. The \log_{10} of EN (left) and histogram of AE (right) in C-Town.

are listed in Table 4. The computational results reported in Table 4 are averaged after testing three times for each network with random initial guesses.

6. Sensitivity Analysis

To study the sensitivity of our approach and demonstrate how accelerated convergence of Algorithm 1 can be achieved, we utilize the Anytown network (Walski et al., 1987). The Anytown network contains 19 junctions, 3 reservoirs, and 40 pipes, as shown in Figure 3b. The corresponding LP modeling has a 63×63 matrix A. Algorithm 1 parameters for Anytown network are set as threshold = 0.01 and maxIter = 5,000. Compared with similar scale networks, the convergence time for Anytown network is relatively slow, requiring 4,995 iterations to reach the threshold. Figure 6 shows the change in the error $\log_{10}(EN)$ with the number of iterations (blue). After analyzing the source data of the Anytown network, we notice that the main errors are caused by the flows through Pipes 78 and 80, connecting the two reservoirs (labeled as blue line segment in Figure 3b). Here, we only show the analysis for Pipe 78 since both pipes have the same parameters.

The first three columns in Table 5 show the results after 200 iterations, including the heads at Reservoir 65 and Junction 60, that is, h_{65} and h_{60} , respectively, the head loss, Δh_{78}^P , and flow, q_{78} , in Pipe 78 connecting Junction 60 with Reservoir 65. Notice that relative error of h_{60} between our final GP-LP solution and EPANET solution is only 0.0092%, however, the relative error of q_{78} up to 55.3611%. Intuitively, the reason for the error stems from the pipe resistance coefficient, R, which is significantly low compared to the rest of the network ($R_{78} = 8.1712 \times 10^{-7}$). The resistance values of all 40 pipes are plotted in Figure 5. From the bar plot, we can see that the resistance coefficients for the other pipes in the network are 100 to 1,000 times greater than for these two pipes. Next, recall the head loss equation (5), rearranging in terms of the flow we get

$$q_{78}^{\mathrm{P}} = \left(\frac{\Delta h_{78}^{\mathrm{P}}}{R_{78}}\right)^{0.54},$$

where resistance coefficient R_{78} is defined by Hazen-Williams. Hence, small difference in $\Delta h_{78}^{\rm P}$ would result in large difference in q_{78} due to the small R. For this reason, flows q_{78} and q_{80} deviate significantly from the EPANET solution. According to the conservation of mass (4), any variables related to q_{78} and q_{80} will be affected.

In order to verify our conclusion that the GP-LP method is sensitive in the resistance coefficients R, we increase $R_{78} = 9.5873 \times 10^{-5}$ by increasing the length, reducing the diameter and the $C_{\rm HW}$ coefficient of the pipe, and compare with updated EPANET simulation results. The corresponding results are shown in the middle three columns of Table 5, and the relative error of q_{78} after 200 iterations is only 0.7278%, where

Table 4 Tested Networks and the Corresponding Computational Time Using Algorithm 1							
Network	Eight node	Anytown	C-Town	PES	NPCL	OBCL	
# of	{9,1,1,	{19,3,0,	{364,1,7,	{68,3,0,	{337,0,2,	{262,1,0,	
componentsa	10,1,1}	40,1,0}	405,11,4}	99,0,0}	399,0,0}	288,1,0}	
# of variables	23	63	783	170	738	552	
# iterations	57	256	729	55	595	87	
Time (sec)	0.0050	0.0553	5.6281	0.0346	4.3761	0.6730	
^a # of components: {# Junctions, # Reservoirs, # Tanks, # Pipes, # Pumps, # Valvesg}							

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Table 5

Sensitivity Analysis for the Anytown Network									
	Base case without a_n			Sensitive analysis			Base case with \boldsymbol{a}_n		
	$\xi_{ ext{GP-LP}}$	$\xi_{ ext{EPANET}}$	RE	$\xi_{ ext{GP-LP}}$	$\xi_{ ext{EPANET}}$	RE	$\xi_{ ext{GP-LP}}$	$\xi_{ ext{EPANET}}$	RE
h ₆₅	215	215	0%	215	215	0%	215	215	0%
h ₆₀	215.1435	215.0342	0.0092%	214.4865	214.4824	0.0019%	215.0362	215.0342	0.0019%
$\Delta h_{78}^{ m P}$	0.1435	0.0342	_	0.5135	0.5176	_	0.0362	0.0342	_
q ₇₈	139.8081	313.1986	55.3611%	-102.8188	-103.5727	0.7278%	307.1522	313.1986	1.93%

updated parameters are referred as case of sensitivity analysis while the previous parameters are marked as base case.

To address the sensitivity problem causing the slow convergence, we utilize the acceleration parameter \boldsymbol{a}_n in Algorithm 1. We test two scenarios: (i) all acceleration parameters are set to 20 and (ii) adjusting the acceleration parameters in each iteration according to (B8). Figure 6 shows the $\log_{10}(\text{EN})$ with the number of iterations without an acceleration parameter (blue), with the same acceleration parameter for all pipes (red), and adjusting the acceleration parameter for Pipes 78 and 80 (yellow). Comparing with the base case without \boldsymbol{a}_n which takes 4995 iterations to converge, using same acceleration parameters converges withing 654 iterations, and with different acceleration parameters converges within 256 iterations. The latter solution is presented in the last three columns in Table 5 and the maximum relative error caused by q_{78} is only 1.93%, which improved significantly compared with the base case.

7. Using GP-NET and Future Extensions

7.1. Using the Proposed WFP Solver: GP-NET

All the codes, tested networks, and results are available on GP-NET (2019). From our formulations, the code of solving WFP can be divided into three categories. The first category is using WFP-GP (26) formulation and can be solved by general GP solvers (Grant & Boyd, 2014; MOSEK ApS, 2014). The second category is formulated based on WFP-LP (30) and can be solved is using LP solvers. The third is the matrix form of LP (31), which needs no solvers, and the analytical solution can be obtained for each iteration. Technically, WFP-GP and WFP-LP are more general, and could be adapted to any other problems such as control and state estimation problems (Wang et al., 2019) in WDNs by simply modifying the objective function or adding constraints, while the analytical solution provided by matrix form of LP is faster and can only be applied to solving the WFP. We note that not all nonlinear functions can be converted into GP form so far, and both WFP-GP and WFP-LP are meaningful since some objective functions are easier to formulate as GP or vice versa. Since all formulations are based on or derived from GP, we name the solver GP-NET. In order to use GP-NET properly, the reader is referred to the Readme.md file on github (GP-NET, 2019).

7.2. Pressure-Driven Modeling

Pressure-driven demand can be seamlessly integrated into the GP modeling approach. The pressure-driven demand function can be formulated as (Giustolisi et al., 2008; Giustolisi & Laucelli, 2011)

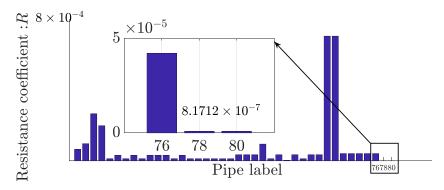


Figure 5. The resistance coefficient *R* for all 40 pipes in Anytown network (Pipes 76, 78, and 80 are magnified for comparison purposes).

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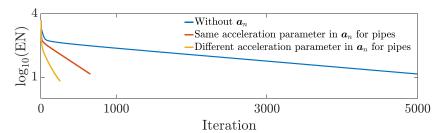


Figure 6. $\log_{10}(EN)$ with the number of iterations (4995, 654, and 256) by adjusting acceleration parameter a_n .

$$d_i^{\text{act}} = \begin{cases} d_i^{\text{dsgn}} & h_i \ge h_i^{\text{ser}} \\ d_i^{\text{dsgn}} \left(\frac{h_i - h_i^{\text{min}}}{h_i - h_i^{\text{min}}} \right)^{\gamma} & h_i^{\text{min}} < h_i < h_i^{\text{ser}} \\ 0 & h_i \le h_i^{\text{min}} \end{cases}$$
(37a)

where d_i^{act} is the actual supplied demand, d_i^{dsgn} is the desired demand, h_i^{ser} and h_i^{min} are the service and the minimum heads, respectively, and γ is typically equal to 0.5 (Wagner et al., 1988).

Given the pressure-driven demand model, the mass balance equation (4) can be rewritten as

$$\sum_{j \in \mathcal{N}_i^{\text{in}}} q_{ji} - \sum_{j \in \mathcal{N}_i^{\text{out}}} q_{ij} = d_i^{\text{act}}.$$
 (38)

The pressure-driven demand is a function of h_i in three different regions. The shape of the demand function for $h_i \geq h_i^{\text{ser}}$ and $h_i \leq h_i^{\text{min}}$ is similar to the original demand-driven formulation (4). For $h_i^{\text{min}} < h_i < h_i^{\text{ser}}$, the demand in (37b) has the similar form of the head loss model $h_i - h_j = R_{ij} \left| q_{ij}^P \right|^\mu$ in (5). In fact, it is easier than the head loss model (5) because (37b) does not have the absolute sign; hence, the same trick we introduced to deal with the head loss model is also applicable. The GP form of (38) can be expressed as

$$\prod_{j \in \mathcal{N}_i^{\text{in}}} \hat{q}_{ji}^{-1} \prod_{j \in \mathcal{N}_i^{\text{out}}} \hat{q}_{ij}^{-1} \hat{h}_i^{-1} \left[\hat{c}^{\mathsf{J}} \right]^{-1} = 1,$$

where $\hat{c}^{J} = b^{h_l - d_l^{act}}$ is a parameter similar as \hat{c}^{P} in the GP form of head loss. The corresponding LP form is written as

$$\sum_{j \in \mathcal{N}_i^{\text{in}}} q_{ji} - \sum_{j \in \mathcal{N}_i^{\text{out}}} q_{ij} - h_i = c^{\mathsf{J}}.$$

Note that c^J is updated similarly as the updating process in (22) and (23), by checking the value of h_i in the previous iteration and selecting the appropriate function d_i^{act} to update the new value of c^J . Nodal leakage can be modeled similarly to (37), having two cases for negative and positive nodal pressure head, and by superimposing leakage from contributing pipes proportionally to the pressure at the incident nodes (Giustolisi et al., 2008).

7.3. Optimal Control

The WFP can be integrated in optimization problems for different applications. For example, consider optimal tank and pump control in WDNs, in which the objective of the operator is to minimize the deviation of the water levels in tanks $\boldsymbol{h}^{\text{TK}}(k)$ from a target value $\boldsymbol{h}^{\text{TK}}_{\text{set}}$ or enforce smooth operation by minimizing the variability of pump operations $\Delta \boldsymbol{q}^{\text{M}}(k)$. These can be added as objective functions to form a WFP-constrained optimization problem formulated in WFP-GP (26) or in WFP-LP (30). Specifically,

$$\Gamma_1(k) = \left(\boldsymbol{h}^{\mathrm{TK}}(k) - \boldsymbol{h}^{\mathrm{TK}_{\mathrm{set}}}\right)^{\mathsf{T}} \quad \left(\boldsymbol{h}^{\mathrm{TK}}(k) - \boldsymbol{h}^{\mathrm{TK}_{\mathrm{set}}}\right)$$
(39a)

$$\Gamma_2(k) = \Delta \mathbf{q}^{\mathrm{M}}(k)^{\mathrm{T}} \Delta \mathbf{q}^{\mathrm{M}}(k), \tag{39b}$$

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where $\Gamma_1(\cdot)$ promotes maintaining the targeted water storage set by the operator; \boldsymbol{h}^{TK} collects the head in tanks, and $\boldsymbol{h}^{TK}_{set}$ is a vector collecting the target head levels of tanks; $\Gamma_2(\cdot)$ promotes the smoothness of control actions through $\Delta \boldsymbol{q}^M(k) = \boldsymbol{q}^M(k) - \boldsymbol{q}^M(k-1)$ by minimizing the variability in the flow rate changes of controllable components from time k-1 to k. We can convert the above objective functions using proposed GP tricks: (1) Conversion of Γ_1 : The objective Γ_1 promotes \boldsymbol{h}^{TK} to be close to $\boldsymbol{h}^{TK_{set}}$. Hence, we introduce a new auxiliary variable $\hat{\boldsymbol{z}}(k) \triangleq \boldsymbol{b}^{h^{TK}_{set}}$ which will be close to $\boldsymbol{1}$ when tank water levels are close to the target levels. Using the epigraph form, the original objective function Γ_1 is replaced with $\hat{\Gamma}_1(\hat{\boldsymbol{z}}(k)) = \prod_{i=1}^{n_t} \hat{z}_i(k)$ and the following constraints are added $\hat{z}_i(k) = \hat{h}_i^{TK_{set}}[\hat{h}_i^{TK}(k)]^{-1}$ and $\hat{z}_i(k) \geq 1$, where $\hat{h}_i^{TK_{set}} = b^{h^{TK_{set}}}$ and $\hat{h}^{TK}(k) = b^{h^{TK}(k)}$. (2) Conversion of Γ_2 : Using the epigraph form, the original objective function Γ_2 can be expressed as a new objective $\hat{\Gamma}_2(\hat{\boldsymbol{p}}(k)) = \prod_{i=1}^{n_m} \hat{p}_i(k)^{\Delta q_i^M(k)}$ with additional constraints given as $\hat{p}_i(k) = \hat{q}_i^M(k)[\hat{q}_i^M(k-1)]^{-1}$ and $\hat{\Gamma}_2(\hat{\boldsymbol{p}}(k)) \geq \beta$ where parameter β stands for the extent of smoothness of the objective function and to prevent $\hat{\Gamma}_2(\hat{\boldsymbol{p}}(k))$ from reducing to 0.

8. Conclusions

In this paper, a new derivative-free, linear approximation method is proposed for solving the WFP. The proposed approach transforms the variables and constraints in WFP, which, ultimately, reduces to an LP that can be solved analytically or by linear solvers. Case studies demonstrate the performance in terms of accuracy and convergence rates. The proposed approach considers looped and branched network topologies, flow directions, and various valve types, it is scalable to large water networks. Under mild conditions, we show that the proposed linear approximation converges and provide guidelines to achieve convergence speedups. Additionally, we demonstrate future extensions to include pressure-driven demand and leak modeling as well as integrating the WFP in network control and state estimation problems. The modeling approach proposed in this work can be transferred to other infrastructure systems, such as natural gas infrastructure, in which the governing equations can be modeled similarly to water networks, where gas flow and pressures correspond to water flow and heads, compressor and regulator stations correspond to pumps and control valves that increase and regulate pressures, respectively (Babonneau et al., 2012; Misra et al., 2015; Pfetsch et al., 2015). Future work will explore possible extensions to other infrastructure systems as well as further improving the computational performance of the proposed approach.

Appendix A: Proof A is Invertible

Proof According to Assumption 1, we know that A_0 is invertible, that is, a row of all zeros does not exist after Gaussian elimination. Hence, the row submatrices in A_0 are linearly independent with each other, which means A_h^R , A_h^{TK} , A_h^P , and A_h^M are linearly independent with each other. According to Remark 2, row submatrices A^J , A^R , A^{TK} , and A^W in A are also linearly independent with each other. Thus, in order to prove A is invertible, we only need to prove A^P and A^M are linearly independent with the other row submatrices in A. We will prove that A^P (corresponding to the pipes) is linearly independent of the rest of the submatrices.

First, we can see that $A^P \in \mathbb{R}^{n_p \times n_p}$ itself is linearly independent because it contains a $I_{n_p \times n_p}$. Second, A^P is linearly independent of A^R , A^{TK} , A^M , and A^W because identity matrix $I_{n_p \times n_p}$ cannot be eliminated with zero rows using Gaussian elimination. Third, it is clear that A^P is linearly independent with A^J because each row in A^P collecting (26) includes linear combination of heads and flows, while each row in A^J collecting (4) includes linear combination of flows. Similarly, we can prove that A^M is linearly independent of the rest of submatrices. Hence, A is invertible.

Appendix B: Convergence of GP-LP Iteration

In this section, we show the convergence of proposed GP method under mild conditions that typically hold in practical WDNs. The theorem and proof are given first, followed by a discussion on how the initial points and acceleration parameter in Algorithm 1 are related with the convergence. Although Algorithm 1 allows checking and updating the status of pumps and valves in each iteration, this section focuses on the typical WFP setting where the statuses are known and, therefore, do not need to be updated in each iteration. In addition, the proof is furnished first for the case where all statuses are open. In this case, GPVs, PRVs, and FCVs have similar modeling of pipes and can be treated directly as pipes with different head loss. This way, we have a WDN with only pumps and pipes, and valves are included in n_m . In what follows, we analyze the iteration $\langle \xi \rangle_n = A^{-1} b$ of Algorithm 1.

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We set aside the effect of acceleration parameter at first; that is, we set $a_n = 0$. Additionally, we combine the equations related with reservoirs and tanks; for example, A^R and A^{TK} are compressed into one row with $h^{R_-TK} = \{h^R, h^{TK}\}, h^{\text{set}} = \{h^{R_{\text{set}}}, h^{TK_{\text{set}}}\}$, and $n_f = n_t + n_r$. Then the matrix in (29) takes the form

$$\begin{bmatrix}
 \frac{A_{11} \mid A_{12}}{A_{21} \mid A_{22}} \\
 A
\end{bmatrix} \xi = \begin{bmatrix}
 0_{n_{j} \times n_{j}} & 0_{n_{j} \times n_{f}} & A_{p}^{J} & A_{M}^{J} \\
 0_{n_{f} \times n_{j}} & I_{n_{f} \times n_{f}} & 0_{n_{f} \times n_{p}} & 0_{n_{f} \times n_{m}} \\
 A_{J}^{T} \mid A_{M}^{R,TKT} \mid -I_{n_{p} \times n_{p}} & 0_{n_{p} \times n_{m}} \\
 A_{M}^{J} \mid A_{M}^{R,TKT} \mid 0_{n_{m} \times n_{p}} & -C_{2}^{M}
\end{bmatrix} \begin{bmatrix}
 h^{J} \\
 h^{R,TK} \\
 q^{P} \\
 q^{M}
\end{bmatrix} = \begin{bmatrix}
 d \\
 h^{\text{set}} \\
 c_{p}^{N} \\
 c_{1}^{M}
\end{bmatrix}.$$
(B1)

Note that \boldsymbol{A} is separated into four blocks, and \boldsymbol{A} changes if and only if $\boldsymbol{C}_2^{\mathrm{M}} = diag(\boldsymbol{c}_2^{\mathrm{M}})$ is updated, where $\boldsymbol{c}_2^{\mathrm{M}} = r(\boldsymbol{q}^{\mathrm{M}})^{\nu-1}$ [cf. (19)] when speed is fixed as \boldsymbol{I} . Similarly, $\boldsymbol{c}_1^{\mathrm{M}}$ is fixed once the pump curve is set, and \boldsymbol{b} changes if only and if $\boldsymbol{c}^{\mathrm{P}} = \log_b(\hat{\boldsymbol{c}}^{\mathrm{P}}) = \boldsymbol{q}^{\mathrm{P}} \circ \left(R|\boldsymbol{q}^{\mathrm{P}}|^{\mu-1} - \boldsymbol{1}\right)$ (4.2.2) is updated. In short, \boldsymbol{A} only reflects the update of pump flows $\boldsymbol{q}^{\mathrm{M}}$, and \boldsymbol{b} only reflects the updates of pipe flows $\boldsymbol{q}^{\mathrm{P}}$.

It follows from $\xi = A^{-1}b$ [cf. (29] that the nth iteration is $\langle \xi \rangle_n = A_{n-1}^{-1}b_{n-1}$, and the n+1th iteration is $\langle \xi \rangle_{n+1} = A_n^{-1}b_n$. Now consider two consecutive iterations n-1 and n, and note that the only changes in A and b are through the updates $\langle C_2^{\rm M} \rangle_n = \langle C_2^{\rm M} \rangle_{n-1} + \langle \Delta C_2^{\rm M} \rangle_{n-1}$ and $\langle c^{\rm P} \rangle_n = \langle c^{\rm P} \rangle_{n-1} + \langle \Delta c^{\rm P} \rangle_{n-1}$. We have $A_n = A_{n-1} + \Delta A_{n-1}$ and $b_n = b_{n-1} + \Delta b_{n-1}$ where $\Delta A_{n-1} = diag(0, \langle \Delta C_2^{\rm M} \rangle_{n-1})$ and $\Delta b_n = [0 \quad 0 \quad \langle \Delta c^{\rm P} \rangle_{n-1} \quad 0]^{\rm T}$. Since we have n_m pumps, we denote the ith element in $\Delta C_2^{\rm M}$ (or the parameter for the ith pump) as $\Delta c_{2,i}^{\rm M}$ and introduce two diagonal matrices U and V defined as follows:

$$\boldsymbol{U} = \begin{bmatrix} \boldsymbol{0}_{(n_h + n_p) \times (n_h + n_p)} & \boldsymbol{0} \\ \boldsymbol{0} & \boldsymbol{I}_{n_m \times n_m} \end{bmatrix}, \quad \boldsymbol{V} = \begin{bmatrix} \boldsymbol{0}_{(n_h + n_p) \times (n_h + n_p)} & \boldsymbol{0} \\ \boldsymbol{0} & \Delta \boldsymbol{C}_2^{\mathrm{M}} \end{bmatrix}.$$
(B2)

With the above notation, we have that $\mathbf{A}_n = \mathbf{A}_{n-1} + \mathbf{U}\mathbf{V}$, where $\Delta \mathbf{A}_{n-1} = \mathbf{U}\mathbf{V}$ is an n_m -rank matrix update. Therefore, we have the iterative formula between two consecutive iterations $\langle \xi \rangle_{n+1} = \mathbf{A}_n^{-1}(\mathbf{b}_{n-1} + \Delta \mathbf{b}_{n-1}) = \mathbf{A}_n^{-1}\mathbf{A}_{n-1}\langle \xi \rangle_n + \mathbf{A}_n^{-1}\Delta \mathbf{b}_{n-1}$, which is written as

$$\langle \xi \rangle_{n+1} = T_n \langle \xi \rangle_n + \boldsymbol{e}_n, \tag{B3}$$

where $T_n = A_n^{-1} A_{n-1}$ and $\boldsymbol{e}_n = A_n^{-1} \Delta \boldsymbol{b}_{n-1}$.

Introducing an appropriate partition for $A_{inv} = A^{-1}$, the vector $e_n = A_n^{-1} \Delta b_{n-1}$ is written as

where $\boldsymbol{A}_{\text{inv22}} = \boldsymbol{A}_{22}^{-1} + \boldsymbol{A}_{22}^{-1}\boldsymbol{A}_{21}[\boldsymbol{A}_{11} - \boldsymbol{A}_{11}\boldsymbol{A}_{22}^{-1}\boldsymbol{A}_{21}]^{-1}\boldsymbol{A}_{12}\boldsymbol{A}_{22}^{-1}$ according to the block matrix inversion theory (Bernstein, 2009). In addition, let $\boldsymbol{A}_{\text{inv}}^{\text{HP,M}}$ denote the entire $(n_h + n_p) \times n_m$ block matrix that sits above $\boldsymbol{A}_{\text{inv22}}^{\text{M}}$.

Attention is now turned to T_n . According to the Sherman-Morrison-Woodbury formula (Woodbury, 1950), we have that

$$\boldsymbol{A}_{n}^{-1} = (\boldsymbol{A}_{n-1} + \boldsymbol{U}\boldsymbol{V})^{-1} = \boldsymbol{A}_{n-1}^{-1} - \boldsymbol{A}_{n-1}^{-1}\boldsymbol{U}(\boldsymbol{I} + \boldsymbol{V}\boldsymbol{A}_{n-1}^{-1}\boldsymbol{U})^{-1}\boldsymbol{V}\boldsymbol{A}_{n-1}^{-1}.$$

Introducing the partitions of A_{inv} from (B4), T_n is written as

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$$T_{n} = I - A_{n-1}^{-1} U (I + V A_{n-1}^{-1} U)^{-1} V = \begin{bmatrix} I & & & & & \\ & I & & -A_{\text{inv}}^{\text{HP,M}} (I + \Delta C_{2}^{\text{M}} A_{\text{inv2}}^{\text{M}})^{-1} \Delta C_{2}^{\text{M}} \\ & & I & & & \\ & & & I - A_{\text{inv2}}^{\text{M}} (I + \Delta C_{2}^{\text{M}} A_{\text{inv2}}^{\text{M}})^{-1} \Delta C_{2}^{\text{M}} \end{bmatrix}$$
(B5)

Remark 3. The entries of $\Delta C_2^{\rm M}$ and $\Delta c^{\rm P}$ can be approximated by $\frac{\partial C_2^{\rm M}}{\partial q^{\rm M}} \Delta q^{\rm M}$ and $\frac{\partial c^{\rm P}}{\partial q^{\rm P}} \Delta q^{\rm P}$.

An assumption that facilitates the convergence analysis of (B3) is introduced next. This assumption is expected to be satisfied for typical values of flows in practical WDNs, and was verified numerically for the WDNs of the numerical tests (section 5).

Assumption 2. Upon defining the matrix $A_f \triangleq diag(\mu R \circ |\mathbf{q}^P|^{\mu-1} - \mathbf{1})$, it holds that $||A_{\text{inv22}}A_f|| < 1$, where ||.|| denotes the spectral norm of a matrix.

The main convergence theorem is stated as follows.

Theorem 1. Under Assumption 2, the GP-LP iteration, or equivalently, the iteration in (B3), converges.

Proof The convergence of vector \mathbf{q}^{P} is shown first. With Remark 3, for the ith pump, $\Delta c_{2,i}^{\mathrm{M}}$ from $\Delta \mathbf{C}_{2}^{\mathrm{M}}$ is obtained from the slope of $c_{2,i}^{\mathrm{M}}$ times the changes in q_{i}^{M} , that is, $\Delta c_{2,i}^{\mathrm{M}} = r(q_{i}^{\mathrm{M}})^{v-2}\Delta q_{i}^{\mathrm{M}} = c_{2,i}^{\mathrm{M}} \frac{\Delta q_{i}^{\mathrm{M}}}{q_{i}^{\mathrm{M}}}$. The typical value of $c_{2,i}^{\mathrm{M}}$ is small due to the fact that parameter r of the pump curve is very small and also renders $\Delta c_{2,i}^{\mathrm{M}}$ even smaller than $c_{2,i}^{\mathrm{M}}$. The typical value of $\Delta c_{2,i}^{\mathrm{M}}$ is thus small enough (10^{-5} m) in practice, which makes the diagonal elements in $\Delta \mathbf{C}_{2}^{\mathrm{M}}$ very small. It follows that the block of \mathbf{T}_{n} that depends on $\Delta \mathbf{C}_{2}^{\mathrm{M}}$ [cf. (B5)] becomes negligible.

Combining the latter with (B5) and (B4), the iteration for the components of q^P in (B3) takes the following form:

$$\langle \boldsymbol{q}^{\mathrm{P}} \rangle_{n+1} = \langle \boldsymbol{q}^{\mathrm{P}} \rangle_n + \langle \boldsymbol{A}_{\mathrm{inv22}} \rangle_n \langle \Delta \boldsymbol{c}^{\mathrm{P}} \rangle_{n-1}.$$
 (B6)

With Remark 3, we have that $\langle \Delta \pmb{c}^{\mathrm{P}} \rangle_{n-1} = diag \left(\mu \pmb{R} \circ |\langle \pmb{q}^{\mathrm{P}} \rangle_{n-1}|^{\mu-1} - 1 \right) \langle \Delta \pmb{q}^{\mathrm{P}} \rangle_{n-1}$. Let $\langle \pmb{A}_{\mathrm{f}} \rangle_{n} \triangleq diag \left(\mu \pmb{R} \circ |\langle \pmb{q}^{\mathrm{P}} \rangle_{n-1}|^{\mu-1} - 1 \right)$, and therefore, (B6) becomes

$$\langle \Delta \boldsymbol{q}^{P} \rangle_{n} = \langle \boldsymbol{A}_{\text{inv22}} \rangle_{n} \langle \boldsymbol{A}_{f} \rangle_{n} \langle \Delta \boldsymbol{q}^{P} \rangle_{n-1} \triangleq \boldsymbol{T}_{n}^{P} \langle \Delta \boldsymbol{q}^{P} \rangle_{n-1}, \tag{B7}$$

where $T_n^{\rm P}=\langle A_{\rm inv22}\rangle_n\langle A_{\rm f}\rangle_n$. Note that each diagonal entry of $A_{\rm f}$ is in [-1,0), indeed, in order for the entries of $A_{\rm f}$ to be outside of the interval [-1,0), it would be required that $|q_{ij}^{\rm P}|\geq \left(\frac{1}{\mu R_{ij}}\right)^{1/(\mu-1)}$. For the typical values of $\mu=1.852$ and $R_{ij}=1\times 10^{-5}$ (unitless) using Hazen-Williams model, the latter condition implies $|q_{ij}^{\rm P}|\geq 24$ CMS, which clearly cannot hold in practical WDNs. Invoking Assumption 2, it follows from (B7) that $\langle \Delta q^{\rm P}\rangle_n \to 0$, which implies that $\langle q^{\rm P}\rangle_n$ converges.

Attention is now turned to the flows through pumps. From the conservation of mass (4), we know that q^M can always be expressed as the linear combination of q^P and demand d, which is fixed. Hence, q^M converges when q^P converges. Next we prove the convergence of the d components of ξ .

From (B1) or original (11), we can obtain $\mathbf{h}^{R_{-}TK} = \mathbf{h}^{set}$ and

$$\begin{bmatrix} \boldsymbol{A}_{p}^{J^{T}} \\ \boldsymbol{A}_{M}^{J^{T}} \end{bmatrix} \boldsymbol{h}^{J} = \begin{bmatrix} \Delta \boldsymbol{h}^{P}(\boldsymbol{q}^{P}) \\ \Delta \boldsymbol{h}^{M}(\boldsymbol{q}^{M}) \end{bmatrix} - \begin{bmatrix} \boldsymbol{A}_{p}^{R-TK^{T}} \\ \boldsymbol{A}_{M}^{R-TK^{T}} \end{bmatrix} \boldsymbol{h}^{R-TK},$$

where $\Delta {\pmb h}^{\rm P}({\pmb q}^{\rm P})$ and $\Delta {\pmb h}^{\rm P}({\pmb q}^{\rm M})$ converge when ${\pmb q}^{\rm P}$ and ${\pmb q}^{\rm M}$ converge. Moreover, ${\pmb h}^{\rm R-TK}={\pmb h}^{\rm set}$ is a constant vector. Hence, we note that the right-hand side is a convergent vector. The size of $[{\pmb A}_{\rm P}^{\rm J} \quad {\pmb A}_{\rm M}^{\rm J}]^{\rm T}$ is $(n_p+n_m)\times n_j$ and it is clear that the number of pipes and pumps is greater than or equal to the number of junctions in a looped network. That is, the matrix $[{\pmb A}_{\rm P}^{\rm J} \quad {\pmb A}_{\rm M}^{\rm J}]^{\rm T}$ has more rows than columns or is a square matrix, and ${\pmb h}^{\rm J}$ which can be expressed by the convergent vector on the right-hand side also converges.

The condition $||T^P|| = ||\langle A_{\text{inv22}} \rangle_n \langle A_f \rangle_n|| < 1$ was valid for all networks we tested and for all n. We observe that two factors impact the convergence of GP iteration, the first one is $\langle A_{\text{inv22}} \rangle_n$ that is mainly decided

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by the network topology, and the second one is the initialization of the flows that is reflected in matrix $\langle \boldsymbol{A}_{\rm f} \rangle_n = diag \left(\mu \boldsymbol{R} | \langle \boldsymbol{q}^{\rm P} \rangle_{n-1} |^{\mu-1} - 1 \right)$. When we initialize the flows as zeros, we have that $\langle \boldsymbol{A}_{\rm f} \rangle_n = \boldsymbol{I}$, which is the worst case. Otherwise, each entry of $\langle \boldsymbol{A}_{\rm f} \rangle_n$ is in (-1,0), which helps making $||\boldsymbol{T}^{\rm P}|| < 1$.

Next, we consider the impact of acceleration parameter \boldsymbol{a}_n in Algorithm 1. If we increase the previous $\langle \Delta \boldsymbol{q}^{\mathrm{P}} \rangle_{n-1}$ by \boldsymbol{a}_n , then we have $\langle \boldsymbol{A}_{\mathrm{f}} \rangle_n = diag \left(\mu \boldsymbol{R} \circ |\langle \boldsymbol{q}^{\mathrm{P}} \rangle_{n-1} + \boldsymbol{a}_n \circ \langle \Delta \boldsymbol{q}^{\mathrm{P}} \rangle_{n-1}|^{\mu-1} - 1 \right)$. In other words, the \boldsymbol{a}_n would impact on $||\boldsymbol{T}^{\mathrm{P}}||$ indirectly via $\langle \boldsymbol{A}_{\mathrm{f}} \rangle_n$. In order to ensure each entry of $\langle \boldsymbol{A}_{\mathrm{f}} \rangle_n$ is in (-1,0) and the updated flow is in $[q_{ii}^{\min}, q_{ii}^{\max}]$, then corresponding \boldsymbol{a}_n for pipe ij is decided by

$$\frac{-(\frac{1}{\mu R_{ij}})^{\frac{1}{\mu-1}} - \langle q_{ij}^{P} \rangle_{n-1}}{\langle \Delta q_{ij}^{P} \rangle_{n-1}} < a_{n} < \frac{(\frac{1}{\mu R_{ij}})^{\frac{1}{\mu-1}} - \langle q_{ij}^{P} \rangle_{n-1}}{\langle \Delta q_{ij}^{P} \rangle_{n-1}},$$
(B8a)

$$\frac{q_{ij}^{\min} - \langle q_{ij}^{\mathrm{P}} \rangle_{n-1}}{\langle \Delta q_{ij}^{\mathrm{P}} \rangle_{n-1}} < a_n < \frac{q_{ij}^{\max} - \langle q_{ij}^{\mathrm{P}} \rangle_{n-1}}{\langle \Delta q_{ij}^{\mathrm{P}} \rangle_{n-1}}.$$
 (B8b)

From the above a_n , we note that (i) a pipe with small R_{ij} could be set with large a_n . $(ii)a_n$ is not only related to the flow rate but also to the change of flow rate in the (n-1)th iteration, and when $\langle \Delta q_{ij}^P \rangle_{n-1}$ converges to zero, a_n can theoretically be infinity. $(iii)a_n$ should be limited by (B8a) and (B8b) simultaneously. The acceleration parameter a_n that is not limited by the above range can cause the iterations to oscillate or diverge, and hence, a large acceleration parameter can make the iterations less stable. It follows that a proper choice of a_n needs be chosen for each element and iteration to reach the best performance of convergence. In practice, we find that the iteration starts to oscillate when a_n is set to a large value, which makes the overall convergence rate to be slower rather than faster. We propose adjusting a_n in each iteration according to (B8), while ensuring that $||T^P|| < 1$, and reduce a_n if the GP iteration start to oscillate. The above guidelines have been verified by Anytown network in section 6. Although beyond the scope of this work, the convergence can be optimized by adopting self-adaptation acceleration parameter (Solomon & Van Hemmen, 1996).

When PRVs or FCVs are in "ACTIVE" statuses, the proof is exactly the same, because the models of active PRVs and FCVs have similar mathematical form as the models of tanks or reservoirs and junctions. For example, when a PRV is active, and the head is set to $\boldsymbol{h}^{R_{\text{set}}}$. That is, $\boldsymbol{A}_h^W \boldsymbol{h} = \boldsymbol{h}^{R_{\text{set}}}$ and $\boldsymbol{b}^W = \boldsymbol{h}^{R_{\text{set}}}$ in (29). In fact, this model is exactly the same as the model of tanks or reservoirs, which is $\boldsymbol{A}_h^{\text{TK}} \boldsymbol{h} = \boldsymbol{h}^{\text{TK}_{\text{set}}}$. Similarly, when a FCV is active, and the flow is set to $\boldsymbol{q}^{R_{\text{set}}}$. That is, $\boldsymbol{A}_W^W \boldsymbol{q} = \boldsymbol{q}^{R_{\text{set}}}$ which is similar to mass balance equation $\boldsymbol{A}_q^J \boldsymbol{q} = \boldsymbol{d}$ in (29). It means we can embed the models of active PRVs or FCVs into (B1) directly, and the proof still holds.

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